



# Electrochemical performance of double-perovskite $\text{Ba}_2\text{MMoO}_6$ ( $\text{M} = \text{Fe}, \text{Co}, \text{Mn}, \text{Ni}$ ) anode materials for solid oxide fuel cells

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## ABSTRACT

Double-perovskite  $\text{Ba}_2\text{MMoO}_6$  ( $\text{M} = \text{Fe}, \text{Co}, \text{Mn}, \text{Ni}$ ) has been systematically investigated as anode materials for solid oxide fuel cells (SOFCs). Among these materials,  $\text{Ba}_2\text{FeMoO}_6$  shows the best electrochemical performance with maximum power density of  $605 \text{ mW cm}^{-2}$  and electronic conductivity of  $196 \text{ S cm}^{-1}$  at  $850^\circ\text{C}$  in  $\text{H}_2$ . Thermal expansion coefficients of  $\text{Ba}_2\text{MMoO}_6$  are distributed within the range of  $(10 - 18) \times 10^{-6} \text{ K}^{-1}$ , matching well with that of  $\text{La}_{0.8}\text{Sr}_{0.2}\text{Ga}_{0.83}\text{Mg}_{0.17}\text{O}_{3-\delta}$  electrolyte. Thermogravimetric analysis (TGA) clearly indicates that oxygen vacancies are formed in all the  $\text{Ba}_2\text{MMoO}_6$  materials. For the  $\text{Ba}_2\text{MMoO}_6$  anodes, the power output decreases in the order of  $\text{M} = \text{Fe} > \text{M} = \text{Co} > \text{M} = \text{Mn} > \text{M} = \text{Ni}$ ; the overpotential increases in the order of  $\text{M} = \text{Fe} < \text{M} = \text{Co} < \text{M} = \text{Mn} < \text{M} = \text{Ni}$ ; and the impedance varies in the order of  $\text{M} = \text{Co} < \text{M} = \text{Fe} < \text{M} = \text{Mn} < \text{M} = \text{Ni}$ . The different performance for this family is ascribed to the difference in conductivity and oxygen vacancy.

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## 1. Introduction

Solid oxide fuel cells (SOFCs) have been studied as advanced power generation devices because of their high energy conversion efficiency, good fuel flexibility and low environmental impact [1–3]. In recent years, SOFCs operating at intermediate temperature (IT, 773–1073 K) or at low temperature are preferable. Running at low temperature can minimize some problems, such as thermal expansion mismatch and chemical reactivity, among the components [4–7]. Pioneering works in IT-SOFCs were carried out with ceria-based oxides. For example, Murray et al. reported that the ceria-containing composite anode delivered a power density of  $370 \text{ mW cm}^{-2}$  at  $650^\circ\text{C}$  in methane by direct electrochemical oxidation [6]; Hibino et al. showed a peak power density as high as  $403 \text{ mW cm}^{-2}$  in SOFC using a ceria-based solid electrolyte at  $500^\circ\text{C}$  in a flowing mixture of ethane and air [7]. However, on the other hand, decreasing the operation temperature will increase the ohmic resistance, reduce the electrode kinetics, and hence decline the output efficiency of the SOFCs.

Conventional electrolyte yttria stabilized zirconia (YSZ) reaches the required conductivity of oxygen ions,  $10^{-1} \text{ S cm}^{-1}$ , at around  $1000^\circ\text{C}$  [8]. The anode-supported SOFCs with thin YSZ electrolyte layer could provide high cell performance at low temperature [9,10]. For example, with  $1\text{-}\mu\text{m}$ -thick YSZ electrolyte, the

thin film SOFCs could obtain maximum power density as high as  $900 \text{ mW cm}^{-2}$  even at  $600^\circ\text{C}$  [9]. However, for thick YSZ electrolyte-supported SOFCs, an operating temperature higher than  $950^\circ\text{C}$  is usually required to achieve sufficient ionic conduction [11]. Working in high temperature may cause thermal degradation and corrosion of the electrode materials, accelerate side reactions occurring at the electrode/electrolyte interface, and hence shorten lifetime of the cell. For the electrolyte-supported SOFCs, lanthanum gallate solid oxides, in particular  $\text{La}(\text{Sr})\text{Ga}(\text{Mg})\text{O}_{3-\delta}$ , are strategic electrolytes to improve intermediate temperature performance. High oxygen ionic conductivities of  $\text{La}(\text{Sr})\text{Ga}(\text{Mg})\text{O}_{3-\delta}$  electrolytes enable their use in IT SOFCs operating at  $600\text{--}800^\circ\text{C}$  [12–14].

Recently, double perovskites have been extensively investigated as alternative SOFC anode materials [15–17]. However, Ba-based double-perovskites have seldom been studied as SOFC anodes. It was reported in our earlier work that substitution at A or B sites in  $\text{A}_2\text{BB}'\text{O}_6$  may impact the oxygen-vacancy concentration and cation valence [17]. As is well known, oxygen-vacancy concentration and cation valence play crucial roles in the properties of the double perovskites [17–19]. In  $\text{Ba}_2\text{MMoO}_6$  ( $\text{M} = \text{Fe}, \text{Co}, \text{Mn}, \text{Ni}$ ), the M-ions are multivalent. With reduction in  $\text{H}_2$ ,  $\text{M}^{3+}$  changes to  $\text{M}^{2+}$  and Mo ions change from +6 to +5; at the same time oxygen vacancies are formed in the structure. The mixed-valent redox couple and the oxygen vacancy are essential to attain expected conductivity and catalytic effect for IT SOFCs.

In this work, Ba-based double perovskites were used as anode materials and  $\text{La}_{0.8}\text{Sr}_{0.2}\text{Ga}_{0.83}\text{Mg}_{0.17}\text{O}_{3-\delta}$  as electrolyte

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for IT-SOFCs. Phase stability, microstructure, thermogravimetric behavior, and thermal expansion were systematically investigated for  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ). The electrochemical performance for the  $\text{Ba}_2\text{MMoO}_6$  anode materials was evaluated in  $\text{H}_2$  fuel at temperatures of 700–850 °C.

## 2. Experimental

$\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) samples were synthesized via a sol–gel method.  $\text{Ba}(\text{CH}_3\text{COO})_2$  (99%),  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (98.5%),  $\text{Co}(\text{CH}_3\text{COO})_2 \cdot 4\text{H}_2\text{O}$  (99.5%),  $\text{Mn}(\text{CH}_3\text{COO})_2 \cdot 4\text{H}_2\text{O}$  (99%),  $\text{Ni}(\text{CH}_3\text{COO})_2 \cdot 4\text{H}_2\text{O}$  (98%) and  $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$  (99%) were used as starting materials. Citric acid served as a complexing agent. The molar ratio of citric acid to the total of metal ions was 2:1. First, citric acid was dissolved into distilled water, and then stoichiometric starting materials were added successively under stirring to achieve a clear aqueous solution. The solution was slowly evaporated on a hot plate for about 20 h to form a gel. The gel was turned into powder after being decomposed at 400 °C in air for 10 h to combust carbonaceous components. The powder was ground in a mortar, and then calcined at 800 °C in air for another 10 h to eliminate the organic substance. The calcined powder was reground, pressed into a pellet with diameter of about 13 mm, and finally sintered to attain the target samples. We found in our experiments that sintering conditions for the four samples are different. For  $\text{Ba}_2\text{FeMoO}_6$  (BFMO) and  $\text{Ba}_2\text{MnMoO}_6$  (BMMO), pure phase cannot be obtained unless being reduced in 5%  $\text{H}_2/\text{Ar}$ . For  $\text{Ba}_2\text{CoMoO}_6$  (BCMO) and  $\text{Ba}_2\text{NiMoO}_6$  (BNMO), pure phase can be achieved by just sintering in air, but impurity  $\text{BaMoO}_4$  appears if being treated in reducing atmosphere. The appearance of  $\text{BaMoO}_4$  will lead to a poor electrochemical performance due to its low conductivity. Therefore, BFMO and BMMO were prepared by sintering in 5%  $\text{H}_2/\text{Ar}$  at 1100 °C for 20 h and 10 h, respectively. BCMO was sintered in air at 1100 °C for 10 h; BNMO was sintered in air at 1200 °C for 10 h. Syntheses of the other materials,  $\text{La}_{0.8}\text{Sr}_{0.2}\text{Ga}_{0.83}\text{Mg}_{0.17}\text{O}_{3-\delta}$  (LSGM),  $\text{SrCo}_{0.8}\text{Fe}_{0.2}\text{O}_{3-\delta}$  (SCF) and  $\text{Sm}_{0.4}\text{Ce}_{0.6}\text{O}_{2-\delta}$  (SDC), have been described in detail elsewhere [19,20]. The starting materials for LSGM were  $\text{La}_2\text{O}_3$  (99.9%),  $\text{SrCO}_3$  (99.0%),  $\text{MgO}$  (99.0%) and  $\text{Ga}_2\text{O}_3$  (99.99%).  $\text{Sr}(\text{NO}_3)_2$  (99.5%),  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (98.5%) and  $\text{Co}(\text{CH}_3\text{COO})_2 \cdot 4\text{H}_2\text{O}$  (99.5%) were used to prepare SCF; whereas  $\text{Ce}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (99.0%) and  $\text{Sm}_2\text{O}_3$  (99.9%) were employed for synthesis of SDC.

Phase purity of the samples was checked at room temperature by X-ray diffraction (XRD) with the Philips X'Pert PRO diffractometer operating with  $\text{CuK}\alpha$  radiation. Rietveld refinement for structure was carried out by using the RIETAN-2000 software. The electrical conductivities of  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) samples were measured from 350 to 850 °C via standard four-probe method on a RTS-8 Digital Instrument under flowing  $\text{H}_2$  (30  $\text{ml min}^{-1}$ ). Redox behaviors of the samples were investigated by thermogravimetric analysis (TGA) obtained in a Stanton STA 781 instrument; the test was operated in 5%  $\text{H}_2/\text{Ar}$  gas flow (100  $\text{ml min}^{-1}$ ) from room temperature (RT) to 900 °C. In the TGA testing, the weight of sample powder was about 15 mg and the heating rate was 10 °C  $\text{min}^{-1}$ .

Single SOFC test cells were fabricated by an electrolyte-supported technique with 300  $\mu\text{m}$  thick LSGM as the electrolyte and SCF as the cathode.  $\text{Ba}_2\text{MMoO}_6$  and SCF were made, respectively, into slurries by using a binder (mass ratio of 10% ethyl cellulose and 90% terpineol). SDC served as a buffer layer between the anode and the electrolyte to prevent the interdiffusion of ionic species between anode and electrolyte [21]. SDC slurry was first screen-printed onto one side of the LSGM disk and fired at 1300 °C in air for 1 h. Then, the  $\text{Ba}_2\text{MMoO}_6$  anode slurry was printed onto the SDC buffer layer and baked in air for 2 h at 1100 °C for BFMO,

BCMO and BMMO, and at 1200 °C for BNMO. The SCF cathode slurry was screen-printed onto another side of LSGM and sintered in air at 1000 °C for 2 h. Here, we need to point out that  $\text{Ba}_2\text{MMoO}_6$  may react with SDC to yield a small amount of  $\text{BaCe}_{1-x}\text{Sm}_x\text{O}_{3-\delta}$  [22]. However, since  $\text{BaCe}_{1-x}\text{Sm}_x\text{O}_{3-\delta}$  has proved to be a potential electrolyte for IT-SOFC [23–25], it will not influence the performance of our cells. Ag paste was used as the current collector for electrochemical testing. The cells were tested in a vertical tubular furnace. The anode side was fed with a flow of pure  $\text{H}_2$  (30  $\text{ml min}^{-1}$ ), and the cathode worked in air. Considering that barium component may thermodynamically react with  $\text{CO}_2$  to form barium carbonate [26], pure  $\text{H}_2$  was produced from electrolysis of purified water in a hydrogen generator rather than reforming gas to avoid formation of barium carbonate.

Electrochemical impedance spectra (EIS) and anodic overpotential of single cells were collected by an electrochemical working station (PARSTAT 2273, Princeton Applied Research, US). Thermal expansion data were attained with a dilatometer Linseis L75H. The power output was measured with an ARBIN FCTS instrument. Power density and current density were calculated by the recorded current flux through the effective area of the cell ( $0.6 \times 0.4 = 0.24 \text{ cm}^2$ ). The secondary electron images of the cells were observed by field-emission scanning electron microscopy (FE-SEM, FEI, Sirion 200) by operation with an accelerating voltage of 10 kV.

## 3. Results and discussion

XRD patterns of  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) samples are shown in Fig. 1a. All the samples show a double-perovskite phase with cubic structure (JCPDF: No. 21-0029); only a small amount of impurity phase  $\text{BaMoO}_4$  appears except for BFMO. Here, it should be noted that the impurity  $\text{BaMoO}_4$  is readily formed during the preparation process. Fig. 1b displays XRD patterns of the samples after testing in  $\text{H}_2$  for 12 h. BFMO shows no change in diffractions before and after reduction in  $\text{H}_2$ , indicating that it is stable in reducing atmosphere. For BMMO and BCMO, a tiny of  $\text{BaCO}_3$  appears after being exposed in  $\text{H}_2$ . The decomposition for BNMO is severe in  $\text{H}_2$ : a large amount of  $\text{BaMoO}_4$  and  $\text{BaCO}_3$  are formed.

All the samples are of cubic structure with space group  $\text{Fm}\bar{3}\text{m}$ . Table 1 displays the unit cell lattice parameters ( $a, b, c$ ), bond lengths, atom occupancy in the lattice ( $g_M$ ), and order parameter ( $\xi$ ) obtained by Rietveld refinement.  $g_M$  reflects proportion of the M ions at their correct sites in the lattice; the value of  $\xi$  can be calculated as  $\xi = 2(g_M - 0.5)$ .  $R_{\text{wp}}$  is reliability factor that reflects the goodness of the refinement. If  $R_{\text{wp}}$  is less than 12%, the refined result is reliable and acceptable.  $R_p$  is profile factor, representing agreement between the observed and calculated profiles. We can see that the bond length  $\langle \text{Fe} - \text{O} \rangle > \langle \text{Mn} - \text{O} \rangle > \langle \text{Ni} - \text{O} \rangle > \langle \text{Co} - \text{O} \rangle$ , which

**Table 1**  
Refined structural parameters, average valence and  $\text{M}^{3+}$  content for  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) at room temperature.

M	Fe	Co	Mn	Ni
Space group	$\text{Fm}\bar{3}\text{m}$	$\text{Fm}\bar{3}\text{m}$	$\text{Fm}\bar{3}\text{m}$	$\text{Fm}\bar{3}\text{m}$
$a = b = c$ (Å)	8.0323(4)	8.0387(9)	8.0307(6)	8.0439(2)
M–O (Å) ( $\times 2$ )	2.132	2.109	2.129	2.110
Mo–O (Å) ( $\times 2$ )	1.934	1.935	1.947	1.927
$R_{\text{wp}}$ (%)	4.732	9.874	8.683	11.073
$R_p$ (%)	4.265	8.364	7.341	9.876
$g_M$	0.939	0.9136	0.924	0.8931
$\xi$	0.878	0.8272	0.848	0.7864
Average valence	2.331(2)	2.206(3)	2.409(1)	2.008(1)
$\text{M}^{3+}$ content (%)	33.1	20.6	40.9	~0

$a, b, c$ : unit cell lattice parameters;  $\xi$ : order parameter;  $g_M$ : atom occupancy in the lattice;  $R_{\text{wp}}$ : reliability factor;  $R_p$ : profile factor.

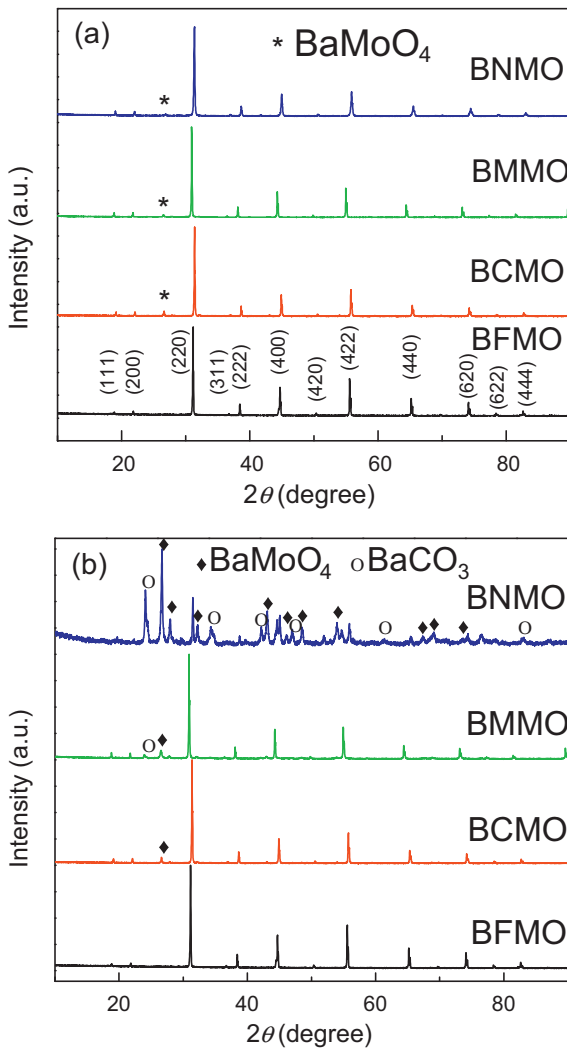
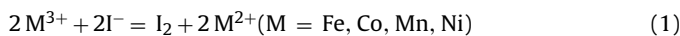


Fig. 1. X-ray diffraction patterns for  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) samples obtained at room temperature: (a) before test and (b) after test in  $\text{H}_2$  for 12 h.

is inconsistent with the order of ionic radii of M ions with high spin in sixfold coordination, i.e.,  $\text{Mn}^{2+}$  (0.83 Å) >  $\text{Fe}^{2+}$  (0.78 Å) >  $\text{Co}^{2+}$  (0.745 Å) >  $\text{Ni}^{2+}$  (0.69 Å) [27]. We used iodometric titration method to measure the valence of the M ions in the as-prepared  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) samples, as described in detail elsewhere [17]. The whole reactions can be expressed as follows:



The average valence and percentage of  $\text{M}^{3+}/M$  ( $M = \text{Fe, Co, Mn, Ni}$ ) are also listed in Table 1. The average valences are 2.331, 2.206, 2.409 and 2.008 for Fe, Co, Mn and Ni ions, respectively. Almost no  $\text{Ni}^{3+}$  ions are detected. The percentages of  $\text{Fe}^{3+}/\text{Fe}$ ,  $\text{Co}^{3+}/\text{Co}$ ,  $\text{Mn}^{3+}/\text{Mn}$  in the samples are 33.1%, 20.6% and 40.9%, respectively. Although the samples were reduced in 5%  $\text{H}_2/\text{Ar}$  for more than 10 h, the  $\text{Fe}^{3+}$  and  $\text{Mn}^{3+}$  contents are still very high. We have found in our previous work that it is impossible to reduce all  $\text{Fe}^{3+}$  ions completely to  $\text{Fe}^{2+}$  in a reducing atmosphere since the band of  $\text{Mo}^{6+}/\text{Mo}^{5+}$  redox couple overlaps with that of  $\text{Fe}^{3+}/\text{Fe}^{2+}$  couple, which consequently prevents the  $\text{Fe}^{3+}$  from being fully reduced [28]. For the same reason,  $\text{Mn}^{3+}$  ions with content as high as 40.9% exist in BMMO. The trivalent ionic radii of M ions with high spin in sixfold coordination are 0.645, 0.645 and 0.61 Å for  $\text{Mn}^{3+}$ ,  $\text{Fe}^{3+}$  and  $\text{Co}^{3+}$ , respectively. As we consider the contribution of  $\text{M}^{3+}$  ions, the

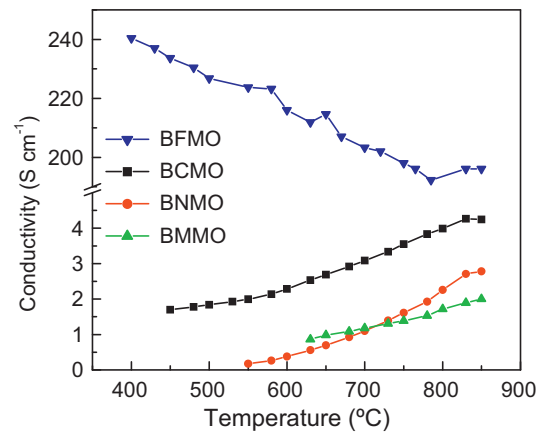


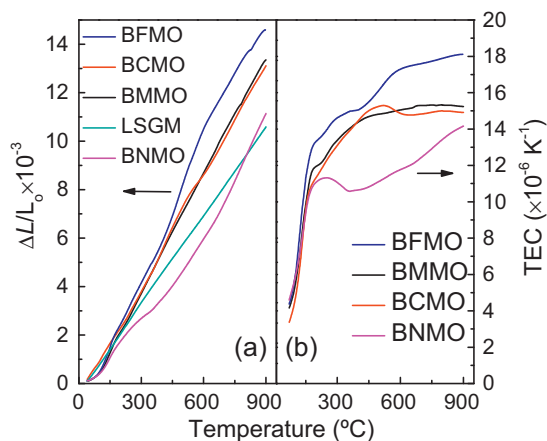
Fig. 2. Temperature dependence of electrical conductivity for  $\text{Ba}_2\text{MMoO}_6$ : (a)  $\text{Ba}_2\text{CoMoO}_6$  (BCMO),  $\text{Ba}_2\text{MnMoO}_6$  (BMMO) and  $\text{Ba}_2\text{NiMoO}_6$  (BNMO) measured in dry  $\text{H}_2$  and (b)  $\text{Ba}_2\text{FeMoO}_6$  (BFMO) measured in dry  $\text{H}_2$ .

order of average length for the (M–O) bonds obtained by refinement agrees perfectly with the  $\text{M}^{2+}$  and  $\text{M}^{3+}$  ionic radii. In addition, the average (Mo–O) bond length strongly depends on the  $\text{Mo}^{5+}/\text{Mo}^{6+}$  ratio that varies with valence state of the M ions and oxygen vacancies.

Fig. 2 shows electrical conductivities measured in dry  $\text{H}_2$  at above 400 °C for the double perovskite samples. The electronic conductivity in perovskite is usually 100–1000 times higher than the oxygen ionic conductivity [29–32]. Therefore, the measured conductivity is mainly referred to electronic conductivity. For an ideal SOFC electrode, it should possess sufficiently high electronic conductivity to ensure efficient current collection. In our measurement, the conductivity of BFMO is as high as  $196 \text{ S cm}^{-1}$  at 850 °C, much higher than those of the other three samples. At 850 °C, the conductivities are 4.2, 2.7 and  $2.0 \text{ S cm}^{-1}$  for BCMO, BMMO and BNMO, respectively. It is interesting that BFMO shows a metal-like behavior whereas the other samples behave as semiconductors and provide small polarization conductivity in the testing temperature range. The small polarization conductivity mechanism is favorable for the cell performance, especially for catalytic activity.

Thermal expansion compatibility between electrolyte and cathode as well as anode is an indispensable consideration for SOFCs. It is necessary for the components to have matchable thermal expansion coefficients (TECs) in the operation temperature range. Thermal expansion incompatibility may cause excessive thermal stress, induce delamination of the electrodes during the sintering and operating processes, and hence reduce the lifetime of the cell [33]. The TECs of the studied anode materials are plotted in Fig. 3 with comparison to that of LSGM. All thermal expansion curves showed a gradual increase in  $\Delta L/L_0$  with increasing temperature. The TEC values at temperatures above 300 °C are distributed within  $(10\text{--}18) \times 10^{-6} \text{ K}^{-1}$ , close to that of LSGM. At temperatures below 300 °C, the thermal expansion behaviors are quite different for the four samples. An obvious change in slope occurs around 300 °C. It has been reported that the thermal expansion for oxygen-deficient perovskites can be contributed to thermal expansion created by atomic vibration of the lattice and chemical expansion associated with change in valence or spin state of the cations [34]. The thermal expansion at low temperatures should be caused by atomic vibrations of the lattice. Therefore, chemical expansion is the main factor that impacts the thermal expansion.

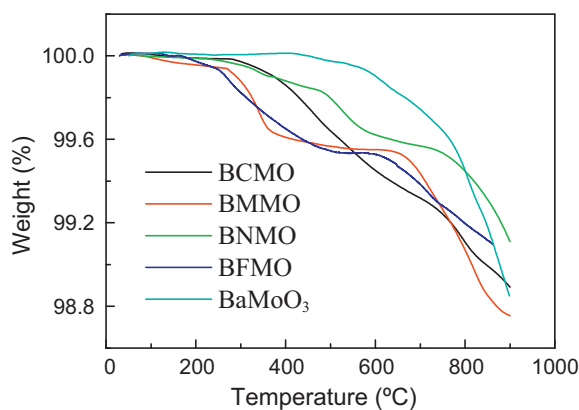
The average TEC of LSGM has been reported to be  $(10\text{--}13) \times 10^{-6} \text{ K}^{-1}$  over 20–900 °C [35]. From Fig. 3, the obtained average TEC of BNMO is  $(10.6\text{--}14.1) \times 10^{-6} \text{ K}^{-1}$  in the temperature range from 300 to 900 °C, which is the lowest among the four anode materials. The TECs of BCMO and BMMO are around  $15 \times 10^{-6} \text{ K}^{-1}$ .



**Fig. 3.** (a) Thermal expansion ( $\Delta L/L_0$ ) and (b) the corresponding thermal expansion coefficients (TECs) as functions of temperature for  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) measured in  $\text{H}_2$  from room temperature to  $900^\circ\text{C}$ .

As compared with the other three samples, BFMO exhibits the highest TEC value, which is  $15.1 \times 10^{-6} \text{K}^{-1}$  at  $400^\circ\text{C}$  and reaches  $18 \times 10^{-6} \text{K}^{-1}$  at  $900^\circ\text{C}$ . All the anode samples show matchable thermal expansion with LSGM electrolyte.

Bernuy-Lopez et al. [36] and Marrero-López et al. [37] reported that reducing  $\text{SrMgMoO}_6$  gave rise to a limited number of oxygen vacancies and some low-valence Mo ions. For anode material, oxygen vacancies facilitate transfer of  $\text{O}^{2-}$  ions that come from the oxide-ion electrolyte, while the mixed-valent  $\text{Mo}^{6+}/\text{Mo}^{5+}$  redox couple results in polaronic conduction to allow transfer of the electrons [15]. Hence, oxygen vacancy and  $\text{Mo}^{6+}/\text{Mo}^{5+}$  redox couple are crucial to attain mixed oxide-ion/electron conducting behavior for the anode. We tested the oxygen vacancies in the as-prepared  $\text{Ba}_2\text{MMoO}_6$  samples by heating the samples in a flowing 5%  $\text{H}_2/\text{Ar}$  atmosphere from room temperature to  $900^\circ\text{C}$ . Fig. 4 presents the recorded TGA curves. The four samples begin to show a tiny weight loss at about  $200^\circ\text{C}$  due to release of  $\text{H}_2\text{O}$ . All samples show an obvious weight loss at  $300^\circ\text{C}$ , which is primarily caused by formation of oxygen vacancies. Since the  $\text{Mo}^{6+}/\text{Mo}^{5+}$  redox couple is at a higher energy level than the  $\text{M}^{3+}/\text{M}^{2+}$  couples ( $M = \text{Fe, Co, Mn, Ni}$ ), reduction of the samples will first reduce the  $\text{M}^{3+}$  to  $\text{M}^{2+}$ . While the reducing process begins,  $\text{O}^{2-}$  ions combine with  $\text{H}^+$  and at the same time oxygen vacancies are formed. The weight loss at around  $300^\circ\text{C}$  can be ascribed to a small amount of oxygen loss from the lattice. The second step of weight loss occurs from  $500^\circ\text{C}$  to  $900^\circ\text{C}$ , which can be attributed to the further formation of oxygen



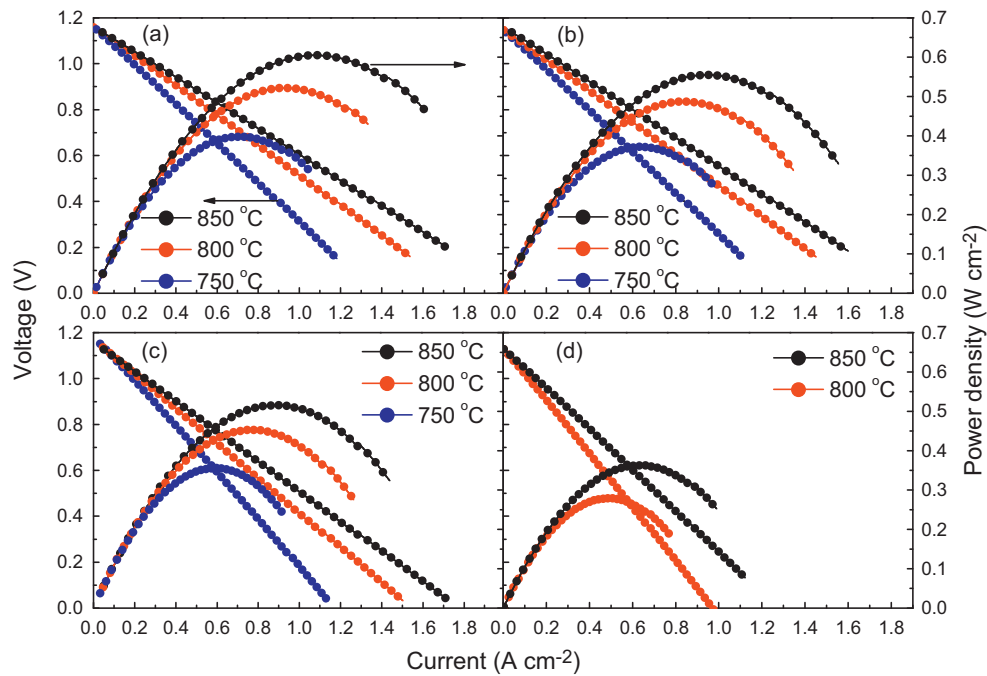
**Fig. 4.** TG curves for  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) recorded from room temperature to  $900^\circ\text{C}$  in 5%  $\text{H}_2/\text{Ar}$  ( $100 \text{ ml min}^{-1}$ ). The curve of  $\text{BaMoO}_3$  is given for comparison.

vacancies accompanied with reduction of  $\text{Mo}^{6+}$  to  $\text{Mo}^{5+}$ . The TG curve of  $\text{BaMoO}_3$  is given for comparison.  $\text{BaMoO}_3$  sample was prepared by the method described in Ref. [38]. For  $\text{BaMoO}_3$ , weight loss caused by reduction of  $\text{Mo}^{6+}$  to  $\text{Mo}^{5+}$  only occurs at temperatures higher than  $500^\circ\text{C}$ . This evidently confirms that for  $\text{Ba}_2\text{MMoO}_6$  samples, the weight loss at around  $300^\circ\text{C}$  is due to the oxygen loss caused by reduction of  $\text{M}^{3+}$  to  $\text{M}^{2+}$ , whereas the weight loss at above  $500^\circ\text{C}$  is due to reduction of  $\text{Mo}^{6+}$  to  $\text{Mo}^{5+}$ . In addition, the weight loss processes for BNMO and BCMO are somewhat different from those for BFMO and BMMO. For BNMO and BCMO, the first weight loss is quite low, and the total weight loss is also low. BNMO and BCMO were prepared by sintering in air. It was reported before that the sample prepared under air shows a small weight decrease below  $800^\circ\text{C}$ , which can be ascribed to a small oxygen loss from the structure [37]. As seen in Fig. 4, the weight loss for BNMO is lowest, which is in accordant with the result of iodometric titration that indicates that almost no  $\text{Ni}^{3+}$  exists in the sample. At  $800^\circ\text{C}$ , the weight percentages are 99.20%, 99.11%, 99.07% and 99.45% for  $M = \text{Fe, Co, Mn}$  and  $\text{Ni}$ , respectively, which means that the yielded oxygen vacancies  $\delta$  for the four samples are 0.23, 0.29, 0.30 and 0.18. BNMO produces the lowest oxygen vacancy in the reducing atmosphere among the four samples.

The double perovskites  $\text{Ba}_2\text{MMoO}_6$  ( $M = \text{Fe, Co, Mn, Ni}$ ) as anode materials were tested with electrolyte-supported single cells (0.3-mm-thick LSGM electrolyte) working in pure  $\text{H}_2$ ; SCF served as cathode with static air as oxygen source. Fig. 5 presents power density and cell voltage as functions of current density at various temperatures in  $\text{H}_2$ . The open circuit voltages (OCVs) are close to the expected Nernst potential 1.2 V. The values of maximum power density ( $P_{\text{max}}$ ) at  $850^\circ\text{C}$  are 555, 515 and  $362 \text{ mW cm}^{-2}$  for BCMO, BMMO and BNMO, respectively. BFMO exhibits the best electrochemical performance with  $P_{\text{max}}$  values of 605, 521 and  $398 \text{ mW cm}^{-2}$  at 850, 800 and  $750^\circ\text{C}$ , respectively. In contrary, the power output for BNMO is lowest. Compared with  $\text{Sr}_2\text{MMoO}_6$  ( $M = \text{Mg, Mn, Fe, Co, Ni}$ ) anodes, the power densities of the present  $\text{Ba}_2\text{MMoO}_6$  are somewhat lower [17,39].

In order to get insight into the cell performance, electrode overpotential was investigated. In general, the overpotential is mainly generated from the catalytic activity of oxygen reduction at the cathode and hydrogen oxidation at the anode, which can be determined by the exchange current density. Fig. 6 shows the overpotential as a function of current density at  $800^\circ\text{C}$  in  $\text{H}_2$  for the double-perovskite anodes. BFMO exhibits the lowest overpotential with about 0.33 V at a current density of  $1.6 \text{ A cm}^{-2}$  at  $800^\circ\text{C}$ . The overpotential increases in the order:  $\text{BFMO} < \text{BCMO} < \text{BMMO} < \text{BNMO}$ , which is exactly consistent with the variation order of the  $P_{\text{max}}$  value and electrical conductivity. The power density strongly depends on the overpotential while the overpotential is greatly influenced by the electrical conductivity. We ascribe the high power output with  $\text{H}_2$  as fuel for the  $M = \text{Fe}$  anode to its high electrical conductivity and low overpotential. For BNMO, the overpotential shows a nonlinear relationship with current density, indicative of the surface-reaction kinetics on the anode probably due to the decomposition of BNMO. The poor power output for BNMO is mainly due to the high overpotential.

Electrochemical impedance spectroscopy (EIS) was further used to evaluate performance of the various electrodes [40–42]. The intercept of the impedance with the real axis in the high frequency range reflects to the ohmic resistance, which can be considered as the electrolyte resistance ( $R_{\text{electrolyte}}$ ) [43]. The intercept of the impedance with the real axis at low frequency corresponds to the total resistance; the radius of the arc corresponds to the anode resistance. We eliminate the ohmic resistance from the total resistances to make an easy comparison of anode polarization resistance. The polarization resistances of  $\text{Ba}_2\text{MMoO}_6$  anodes are obtained directly from the difference between the intercepts at high- and

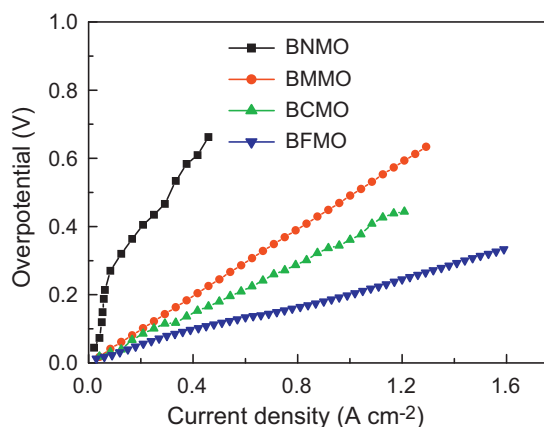


**Fig. 5.** Cell voltage and power density as functions of current density for the cells with  $\text{Ba}_2\text{MMoO}_6$  as anodes: (a)  $\text{Ba}_2\text{FeMoO}_6$ , (b)  $\text{Ba}_2\text{CoMoO}_6$ , (c)  $\text{Ba}_2\text{MnMoO}_6$ , and (d)  $\text{Ba}_2\text{NiMoO}_6$ .

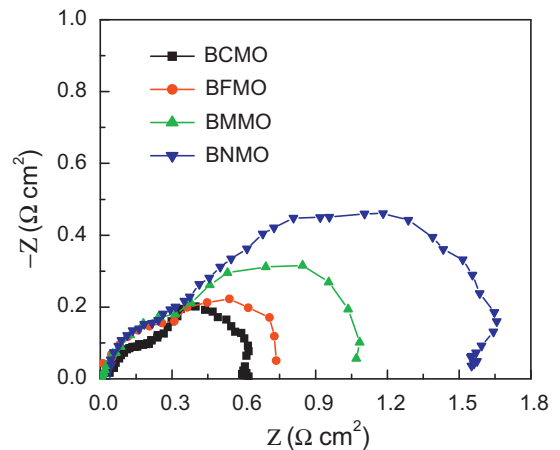
low frequency on the real axis of the impedance plots. Fig. 7 shows the impedance measured under open-circuit condition at  $800^\circ\text{C}$  in  $\text{H}_2$  for the  $\text{Ba}_2\text{MMoO}_6$  anodes. The size of the impedance arcs for the anodes increases with the M-ions in the order of  $\text{BCMO} < \text{BFMO} < \text{BMMO} < \text{BNMO}$ . For the four anodes, the high frequency curves show little difference; the main difference appears in the low frequency range that represents for the absorption and dissociation of  $\text{H}_2$  on the anode surface [44]. The polarization resistances at  $800^\circ\text{C}$  are 0.61, 0.73, 1.07 and  $1.55 \Omega \text{cm}^2$  for BCMO, BFMO, BMMO and BNMO, respectively. Here, it should be noted that the BCMO anode shows the lowest polarization resistance, which is probably due to the high catalytic effect in  $\text{H}_2$  of cobalt ions. Although there are several factors that may contribute to the difference in the impedance, such as grain boundary area [45] and thickness of the anode coating layer, we surmise that the main reason for the difference in our system is the catalytic effects of the anode materials.

Fig. 8 shows the secondary electron images of typical BFMO electrode, SDC buffer layer and LSGM electrolyte after operation of the

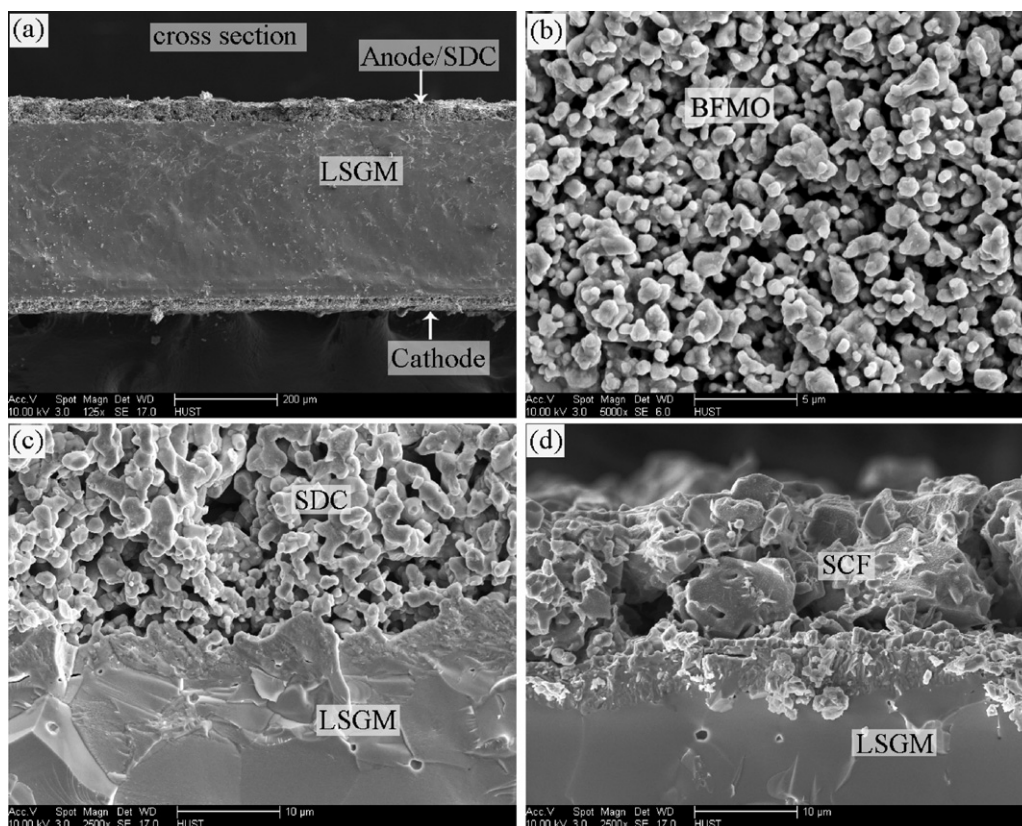
cells. We can see that all of them show clear interfaces after running in  $\text{H}_2$ . Fig. 8a takes BFMO cell as an example to show the cross section of the cell configuration. The thickness of LSGM electrolyte is about  $300 \mu\text{m}$ . Fig. 8b shows the morphology of BFMO anode layer on the disk of LSGM electrolyte. BFMO exhibits a fine and uniform microstructure with an estimated 30% porosity, which benefits surface adsorption and diffusion for fuels and provides sufficient spots for electrochemical reactions. Fig. 8c shows the cross section between LSGM and SDC buffer layer and Fig. 8d shows the cross section between LSGM and SCF cathode. The upper portion shows the porous SCF cathode, and the bottom portion is the micrograph of the dense LSGM electrolyte. The porous SDC buffer layer and SCF cathode connect tightly with LSGM electrolyte. The observed porous microstructure for BFMO, SDC and SCF, uniform particle distribution and tight connection with LSGM electrolyte give rise to sufficient availability of three phase boundaries for charge and



**Fig. 6.** Overpotential as a function of current density for the cells with  $\text{Ba}_2\text{MMoO}_6$  (M = Fe, Co, Mn, Ni) anodes operating at  $800^\circ\text{C}$  in  $\text{H}_2$ .



**Fig. 7.** Interfacial polarization resistances of  $\text{Ba}_2\text{MMoO}_6$  (M = Fe, Co, Mn, Ni) determined from the impedance spectra and resistances of the single cells measured at  $800^\circ\text{C}$  in  $\text{H}_2$  under open-circuit conduction.



**Fig. 8.** SEM images: (a) cross section of cell with configuration of BFMO/SDC/LSGM/SCF after running in  $H_2$ , (b) BFMO sintered at  $1100^\circ C$  on LSGM disk for 2 h, (c) cross section between LSGM and SDC buffer layer, (d) cross section between SCF cathode layer and LSGM electrolyte.

oxygen-ion transfer, which can ensure the cells to present preferable electrochemical performance.

#### 4. Conclusions

Double-perovskites of the type  $Ba_2MMoO_6$  ( $M = Fe, Co, Mn, Ni$ ) have been used as alternative anode materials for SOFCs. In reducing atmosphere, BFMO, BCMO and BMMO are stable, while BNMO is readily decomposed into  $BaMoO_4$  and  $BaCO_3$ . The electronic conductivities and thermal expansions differ greatly for the four materials. BFMO shows excellent electronic conductivity with magnitude as high as  $196 S cm^{-1}$  in dry  $H_2$  at  $850^\circ C$ . TGA curves indicate that all the  $Ba_2MMoO_6$  samples can lose a limited amount of oxygen to yield oxygen vacancy in reducing atmosphere. Among the cells with  $Ba_2MMoO_6$  as anodes and LSGM as electrolyte, the BFMO cell exhibits the highest power output with a maximum power density of  $605 mW cm^{-2}$  in  $H_2$  at  $850^\circ C$ , and the electrochemical performance of the BNMO cell is poorest. The difference in the properties is caused by the difference in conductivity and catalytic effect, which is in nature due to the oxygen vacancy as well as  $M^{3+}/M^{2+}$  and  $Mo^{6+}/Mo^{5+}$  redox couples.

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